

# H<sub>2</sub>SO<sub>4</sub> Catalysis: Perspective and Opportunities for Reducing SO<sub>2</sub> Emissions

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## Abstract

**Introduction:** Development of next-generation chemical processes that have zero emissions is a key environmental objective for sustainable development. The manufacture of H<sub>2</sub>SO<sub>4</sub> by the air oxidation of SO<sub>2</sub> to SO<sub>3</sub> is an important technology where an opportunity exists for new catalyst development and process innovation by reducing emissions of unconverted SO<sub>2</sub> in process reactor tail gases owing to the sheer number and scale of typical plants [1]. Emissions control technologies using new catalyst technology, improved reactor designs, and process strategies have notable potential. The primary objective of this study is two-fold: (1) to review current particulate H<sub>2</sub>SO<sub>4</sub> catalysts utilized in the oxidation of SO<sub>2</sub> to SO<sub>3</sub>; and (2) to develop a COMSOL Multiphysics® simulation to compare the effect of species flux model on catalyst performance for typical process conditions.

**Methods:** COMSOL software is used to model the effect of different species flux models on transport-kinetic interactions in various particulate catalyst geometries. This builds upon our previous work on modeling of transport-kinetic interactions in SO<sub>2</sub> oxidation catalysts shapes [2]. Various diffusion flux models, namely, the Wilke model, the Wilke-Bosanquet, and the Dusty Gas model are not available in COMSOL so these were coded to compare the particle concentration and temperature profiles as well as the particle effectiveness factor over typical process conditions encountered in multi-pass converter operation. The reaction kinetic model is based upon the work of Collina et al. [3] since it accounts for the dependence of the SO<sub>2</sub> oxidation rate on the partial pressures of SO<sub>2</sub>, O<sub>2</sub>, and SO<sub>3</sub>. The Chemical Reaction Engineering Module is used to evaluate adiabatic reactor performance under ideal reactor conditions.

**Results and Discussion:** Typical adiabatic 4-pass converter profiles are shown in Figure 1. These are based upon the Chemical Reaction Engineering Module to describe adiabatic reactor performance with ideal plug flow of the gas. These results provide the incentive for developing new catalyst technology because the maximum SO<sub>2</sub> conversion possible is 99.7%, which is adequate to meet current EPA regulations for SO<sub>2</sub> emissions. However, it does not meet the anticipated future need to design H<sub>2</sub>SO<sub>4</sub> plants with SO<sub>2</sub> emissions < 100 ppm, or even < 10 ppm.

Additional results that compare the performance of particulate catalyst shapes using typical process conditions will be presented and discussed, thereby showing the incentive for

development of alternate catalyst forms with higher activity and reduced emissions.

Conclusions: COMSOL software provides a convenient platform for quantifying detailed transport-kinetic interactions in commercial catalyst particles having complex shapes. The model-predicted results provide a realistic basis for comparison to experimental data. The results show that the observed catalyst performance is notably affected by the choice of diffusion flux model.

## Reference

1. British Sulphur Consultants. "Sulphuric Acid: Global Supply and Demand in the Next Decade." Topsøe Catalysis Forum, Denmark, August 23rd to 24th 2007.
2. Nagaraj, A., & Mills, P. L. "Analysis of Heat, Mass Transport, and Momentum Transport Effects in Complex Catalyst Shapes for Gas-phase Heterogeneous Reactions Using COMSOL Multiphysics". Paper Presented at the COMSOL Conference 2008 Boston, MA.
3. Collina, A., Corbetta, D. and Cappelli, A. "Use of Computers in the Design of Chemical Plants," 97th Event of the European Federation of Chemical Engineering, Firenze (1970).

## Figures used in the abstract

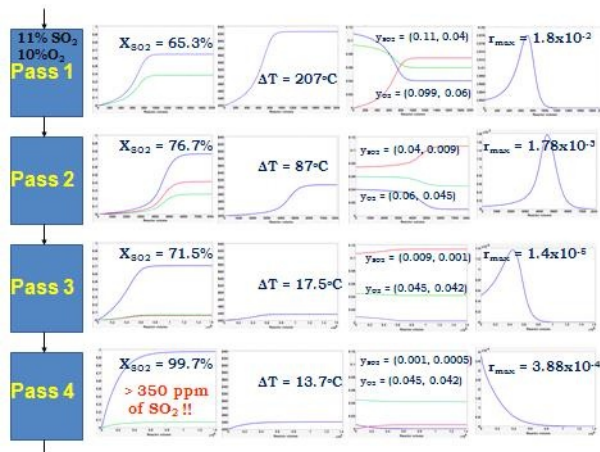


Figure 1: Adiabatic 4-pass converter profiles.