

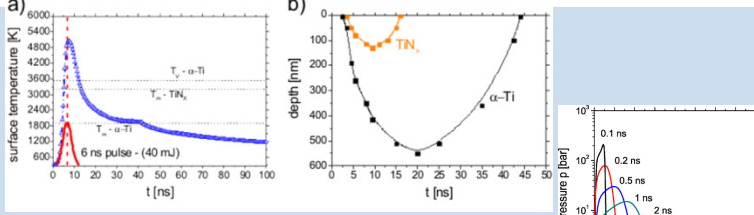
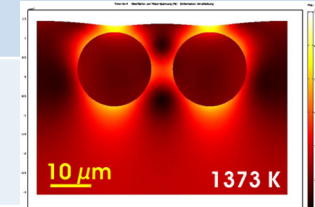
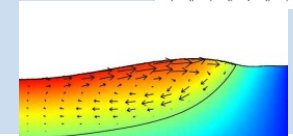
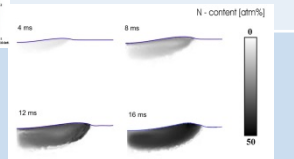
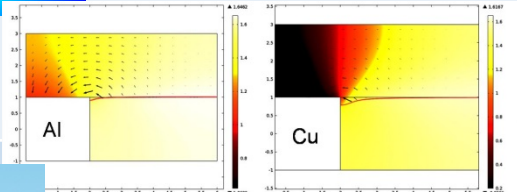
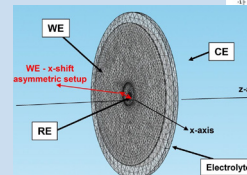
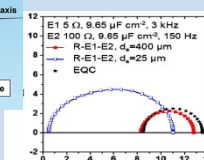
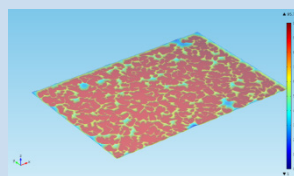
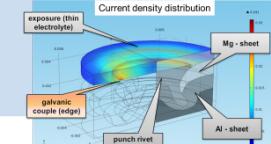
FEM based studies of a Mg/Al hybrid component joint regarding corrosion prediction

Dr. Daniel Höche

Helmholtz-Zentrum Geesthacht

24th October 2013

Comsol History

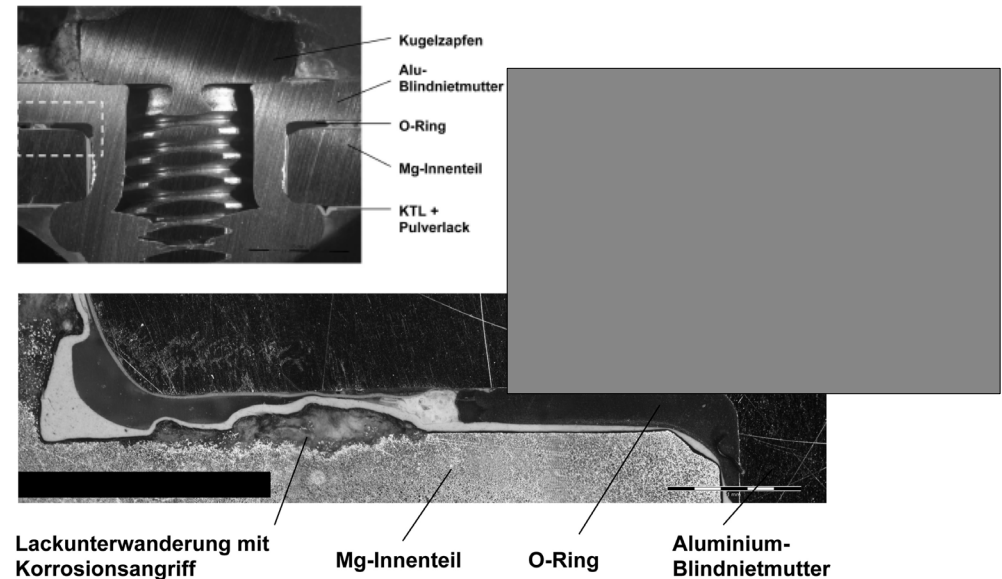
Year	Reference	Image
2007	<p>D. Höche, M. Shinn, J. Kaspar, G. Rapin and P. Schaaf, Laser pulse structure dependent texture of FEL synthesized TiN_x coatings; Journal of Physics D: Applied Physics, Vol. 40(3): 818-825, 2007.</p> <p>D. Höche, G. Rapin and P. Schaaf, FEM simulation of the laser plasma interaction during laser nitriding of titanium; Applied Surface Science, Vol. 254(4): 888-892, 2007.</p>	 <p>Graph (a) shows surface temperature [K] vs time [ns] for a 6 ns pulse. Graph (b) shows depth [nm] vs time [ns] for TiN_x and $\alpha-Ti$ layers. An inset shows pressure p [Bar] vs surface distance y [μm] for various pulse durations (0.1 ns to 20 ns).</p>
2008	<p>P. Schaaf C. Lange, V. Drescher, J. Wilden, D. Höche and H. Schikora, Laser clad surfaces for shark skin effect by high temperature activation; Surface and Coatings Technology, Vol. 203 (5-7): 470-475, 2008.</p>	
2009	<p>D. Höche, M. Shinn, S. Müller, G. Rapin and P. Schaaf, Marangoni convection during free electron laser nitriding of titanium; Metallurgical Material Transaction B, Vol. 40(4): 497-507, 2009.</p>	 
2012	<p>D. Höche and J. Isakovic, Level-set modeling of galvanic corrosion of magnesium; Mg2012 conference in Vancouver, Symposium Simulation and Modeling, 08.-13.07.2012, Proceedings 2012.</p>	
2013	<p>S. Klink, D. Höche, F. La Mantia, W. Schuhmann; FEM modelling of a coaxial three-electrode test cell for electrochemical impedance spectroscopy in lithium ion batteries, Journal of Power Sources, Vol. 240: 273-280, 2013</p> <p>D. Höche and J. Isakovic; Mikrogalvanische Korrosion am Magnesium-Aluminium System - Detaillierte elektrochemische Einblicke mittels FEM - Simulationen, Chemie Ingenieur Technik, online, 2013.</p> <p>D. Höche; Towards the simulation based design of Mg/Al hybrid component joints in terms of corrosion prevention, Proceedings EuroCORR, Estoril, 2013.</p>	   

Corrosion in multi-material design

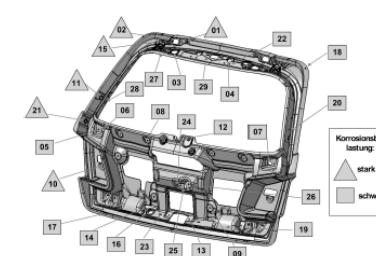
- galvanic corrosion (AA, Mg, Steel, CFK)
- under paint corrosion
- crevice corrosion (gap, edge, scratch)
- localised corrosion / filiform corrosion

Anti-corrosive lightweight design needs:

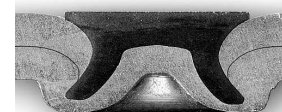
- Constructive corrosion protection
 - component selection (non-metallic)
 - avoiding galvanic contacts
 - spacer distances etc.
- Active corrosion protection
 - optimized coating systems (hybrid)
 - superior pre-treatments
- Corrosion resistant materials / alloys



H. Schreckenberger, P. Izquierdo, S. G. Klose, D. Höche et al.; Materialwissenschaft und Werkstofftechnik, 2010.



P. Izquierdo, S.G. Klose, D. Höche, et al.; World Magnesium Conference. Hongkong, 2010.



by Tucker GmbH

Aims of simulation action

Application on engineering tasks

- Assisting engineers in Multi-Material-Design (combination of different materials) under corrosion protection aspects
- Corrosion prediction for **Multi-Material-Joints** (*welds, rivets, clinches*) = minimising the need of corrosion protection action (*coatings, etc.*)
- Tailoring of various properties like spacing distances

Most common advantages

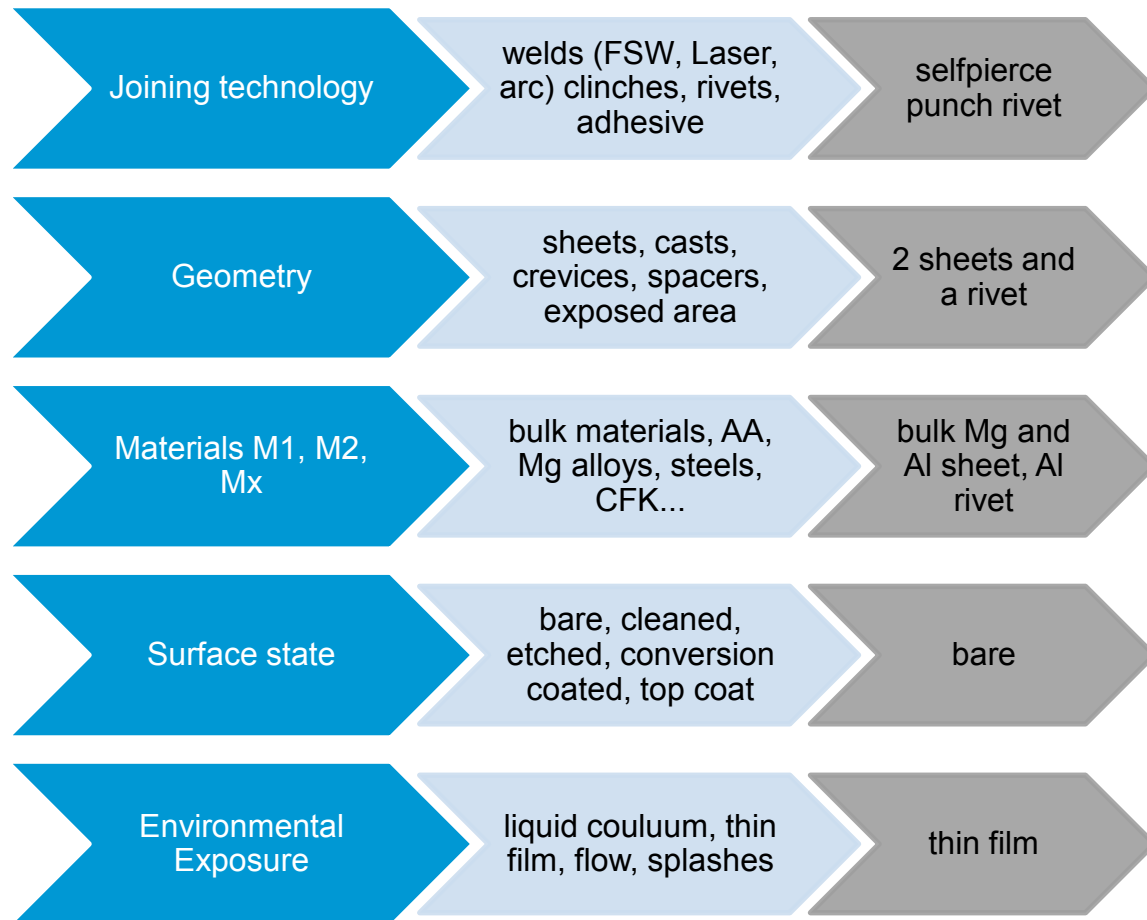
- Reduction of development expenses and periods
- Improved planning ability due to tailored properties
- Simulation based safeguarding of corrosion protection action

Objective:

Computer-Aided Engineering (CAE) in terms of corrosion protection

Anti-corrosive simulation based design

1. Challenge → the model development chain

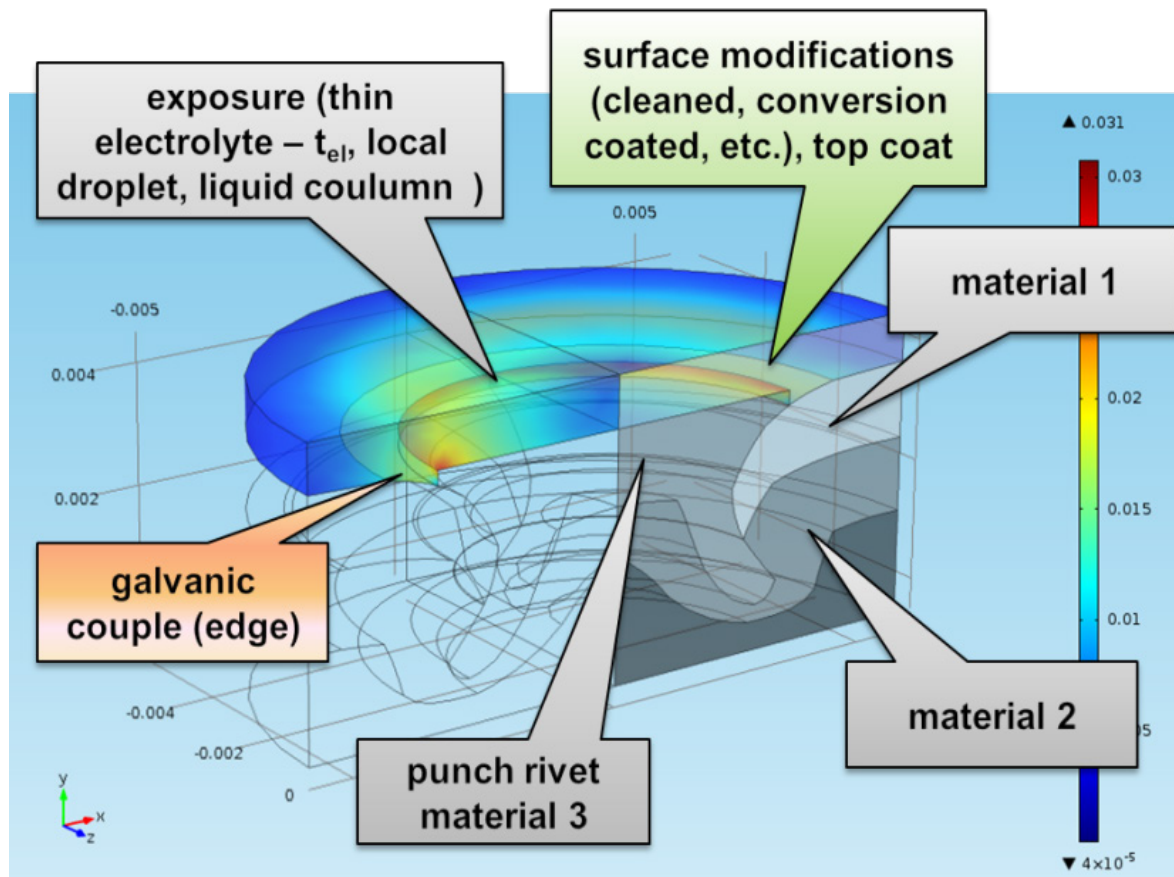


scientific aspects

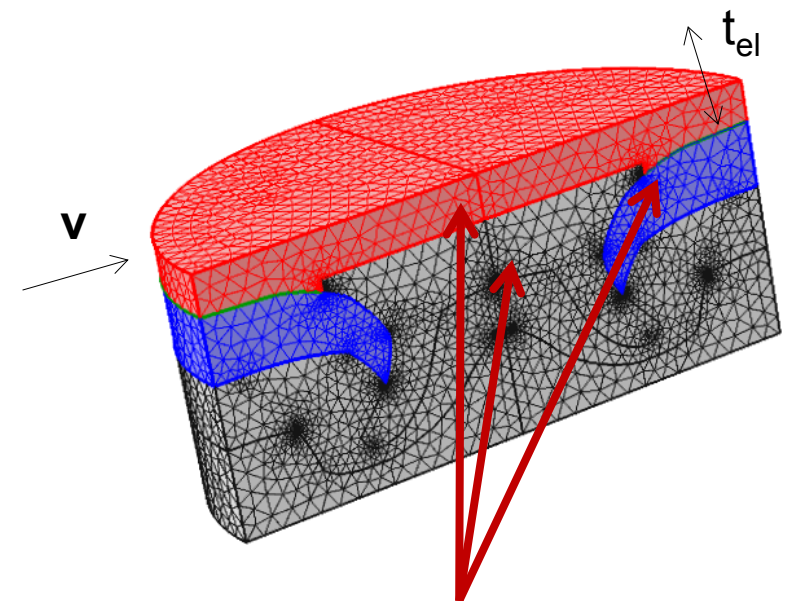
- | |
|--|
| <ul style="list-style-type: none"> • materials state (as received) • scratches, artefacts • Impurities |
| <ul style="list-style-type: none"> • galvanic corrosion • crevices • under paint corrosion |
| <ul style="list-style-type: none"> • electrical properties (conductivity) • electrochemical response |
| <ul style="list-style-type: none"> • interface chemistry • Faraday reaction • passivation, layer growth |
| <ul style="list-style-type: none"> • ion concentration, pH • conductivity • transport mechanism |

Chose the **correct** interdisciplinary approach including the correct physics / chemistry

Self-pierce punch rivet model problem (Al in Mg)



Geometry setup:
use symmetries

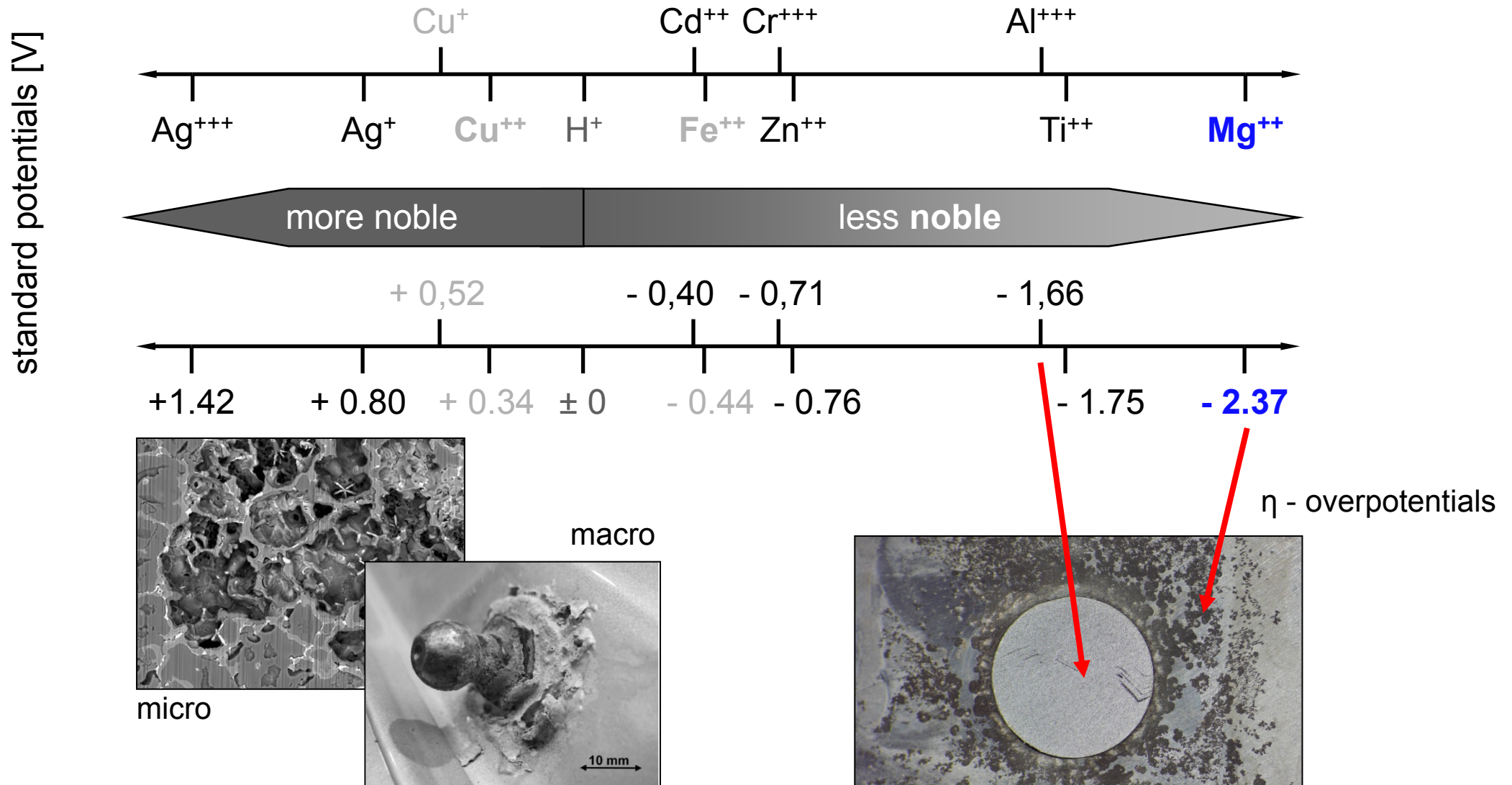


reduce to “active” domains

- Try to figure out **all** aspects → develop the model starting with most “weighted” issue.
- Keep it **as easy as possible** (checking requirements in context to limitations and assumptions)

Most „weighted“ problem

Galvanic couples in Mg based engineering



General rules – galvanic couples

- **ratio of cathode area to anode area / area rule**
- galvanic corrosion will **become more severe** over time once it is initiated.
- affected zone can be relatively large and galvanic corrosion may be caused by a **remote cathode metal** (spacing aspects).
- **avoid** that the anode is **electrically connected** to the cathode (not possible).
- relative positions of electrodes → corrosion products from the Mg anode can be transferred to the cathode, corrosion could be slightly reduced through an “**alkalisation effect**”. (being simulated)
- Corrosion products from the cathode on the Mg surface (e.g. by convection) leading to a “**passivation**” or “**poisoning**” effect, which could either slightly, ameliorates or deteriorates the galvanic corrosion. (very important)
- A “**shortcut**” effect can be caused by the accumulation of corrosion products → accelerating galvanic corrosion unexpectedly at a remote area.

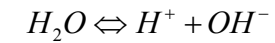
G. Song, B. Johannesson, S. Hapugoda, D. StJohn, Corrosion Science. 46 (2004) 955-977.

Mathematical approach

Nernst:

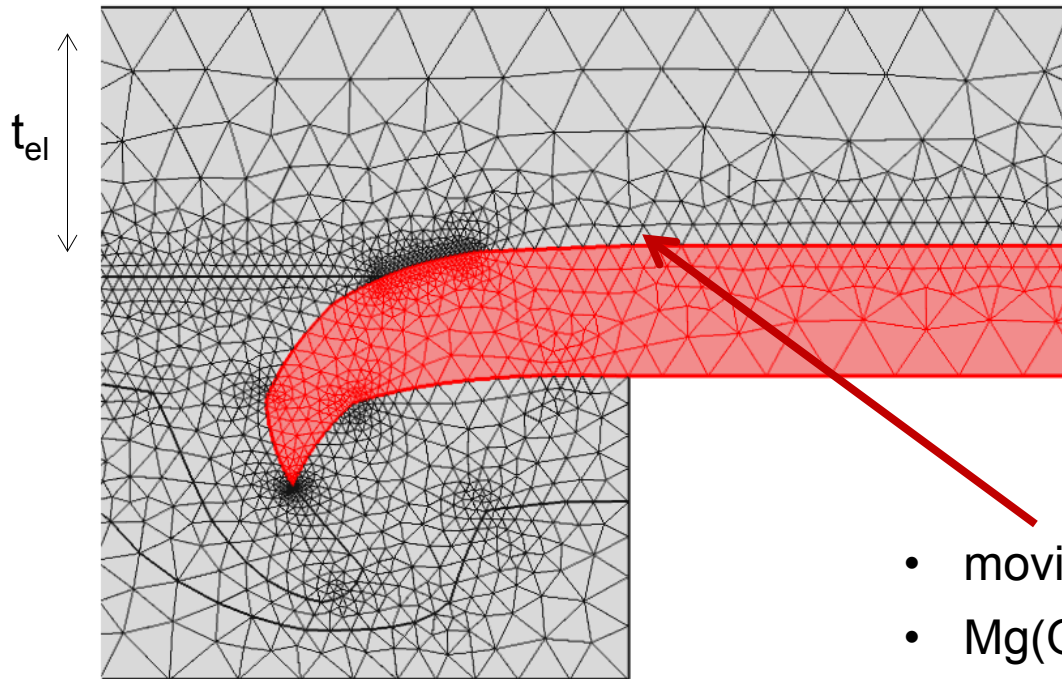
$$\frac{\partial c_i}{\partial t} + \nabla \cdot (-D_i \nabla c_i - z_i \mathbf{u}_{mob} F c_i \nabla U_{el}) + \mathbf{u} \cdot \nabla c_i = R_{i,tot}$$

water autoprotolysis



$$R_{OH^-} = R_{H^+} = k_f - k_b(c_{H^+} c_{OH^-})$$

Faraday:



$$j_{el} = F \sum z_i N_i$$

$$i_{el} = -\sigma \cdot \nabla U$$

- moving interface
- $Mg(OH)_2$ precipitation
- anodic dissolution

Specimens:
(to be extended)

species	Mg^{2+}	OH^-	H^+	Na^+	Cl^-	O_2
D [m^2/s]* 10^{-9}	0.71	5.27	9.31	1.33	5.27	1.98
C_0 [mol/ m^3]	0	10^{-4}	10^{-4}	42	42	0.233

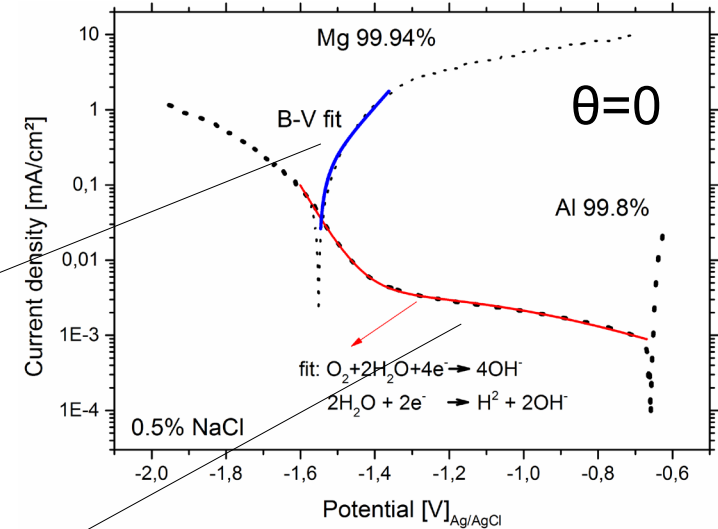
Mathematical approach

to be used: (in 4.2a)

- Tertiary Current Distribution, Nernst-Planck Interface
 - modified boundary conditions (weak form) to include the reduced flux due to layer growth
- Surface Reactions Interface
- Deformed Geometry and Moving Mesh Interface (ALE)
- Mathematics Interface
 - 3 ODE's for surface coverage, layer thickness and porosity

Boundary conditions – electrode response

anodic: Mg dissolution	$Mg \rightarrow Mg^{2+} + 2e^-$
cathodic: oxygen reduction water electrolysis	$O_2 + 2H_2O + 4e^- \rightarrow 4OH^-$ $2H_2O + 2e^- \rightarrow H_2 + 2OH^-$
global reaction:	$Mg + 2H_2O \rightarrow Mg^{2+} + 2OH^- + H_2$

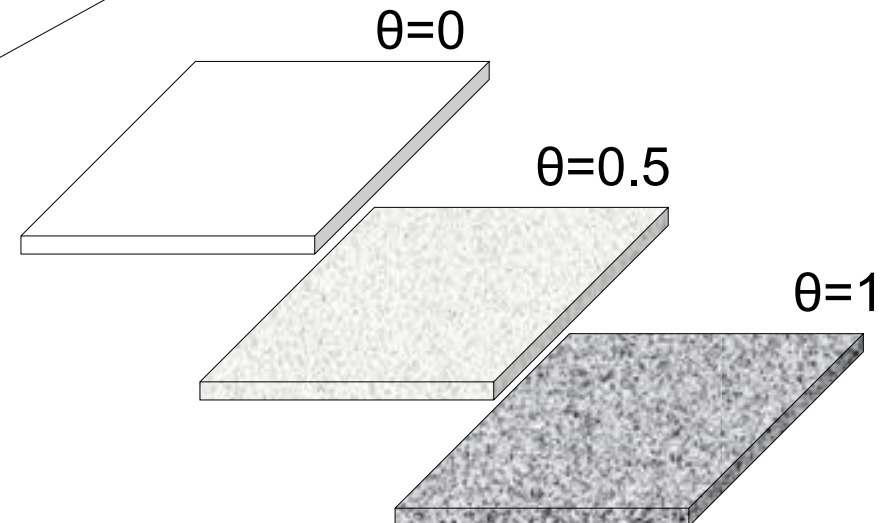


$$i_{anode} = (1 - \theta + \varepsilon\theta) \cdot i_0 \left(e^{\left(\frac{z\alpha_a F\eta}{RT}\right)} - e^{\left(\frac{-z\alpha_c F\eta}{RT}\right)} \right)$$

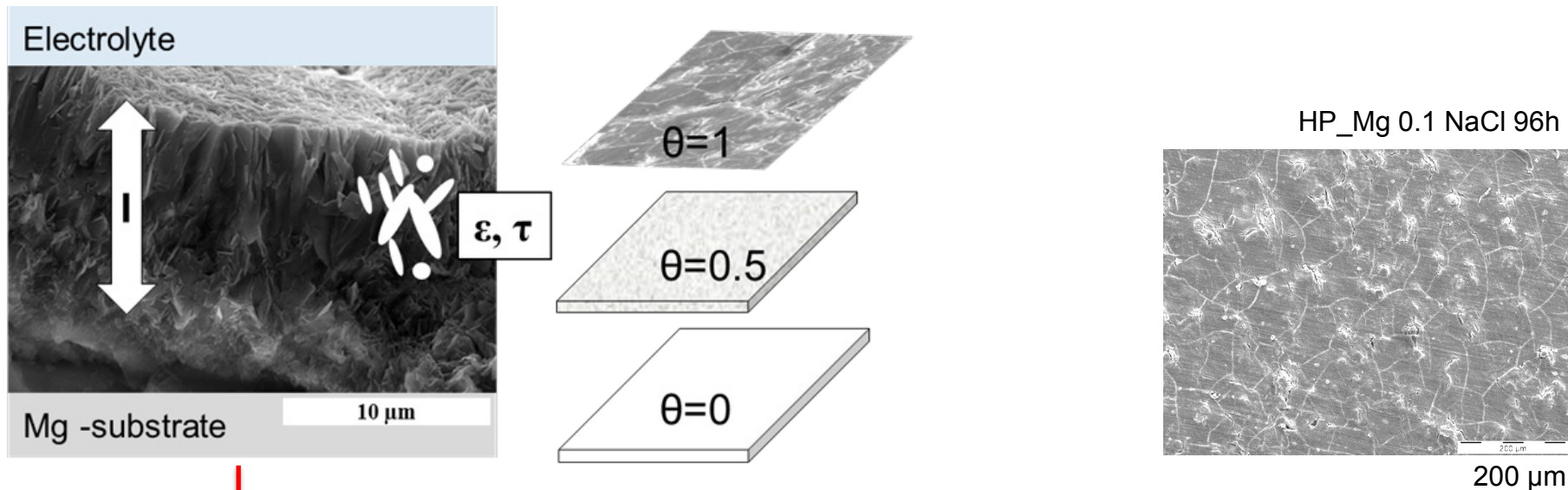
→ Tafel does not work

$$i_{cathode} = (1 - \theta + \varepsilon\theta) \cdot \frac{i_0 e^{\left(\frac{-z\alpha_c F\eta}{RT}\right)}}{1 - \left(\frac{i_0}{i_d}\right) \left[1 - i_0 e^{\left(\frac{-z\alpha_c F\eta}{RT}\right)} \right]} + (1 - \theta + \varepsilon\theta) \cdot i_{0H} \cdot 10^{\left(\frac{-\eta_H}{\beta}\right)}$$

→ self induced corrosion layer growth



Boundary conditions – surface coverage



Surface coverage θ :

$$\frac{d\theta}{dt} = -\frac{1}{l(1-\varepsilon)} \left(\frac{R_{Mg^{2+}} M_{Mg(OH)_2}}{\rho_{Mg(OH)_2}} \right) \quad R_{Mg^{2+}} = -(1-\theta) k_{Mg(OH)_2} (c_{Mg^{2+}} c_{OH^-}^2 - K_{Mg(OH)_2})$$

Reduced flux:

$$\mathbf{n} \cdot (\mathbf{N}_{total} - \mathbf{N}_{eff})_i = \mathbf{n} \cdot \mathbf{N}_{i-red} = D_i \left(\theta - \frac{\theta}{N_M} \right) \left(-\nabla c_i - \frac{z_i F}{RT} c_i \nabla U_{el} \right)$$

Interface velocity:

$$\mathbf{u}_{total} \cdot \mathbf{n} = \underbrace{-\frac{M}{zF\rho} \cdot i_{Mg}(\theta)}_{\text{anodic dissolution}} + \underbrace{u_{layer}}_{\text{deposit growth}} \quad \text{with } u_{layer} = \frac{R_{Mg(OH)_2} M_{Mg(OH)_2}}{(1-\varepsilon)\rho_{Mg(OH)_2}}$$

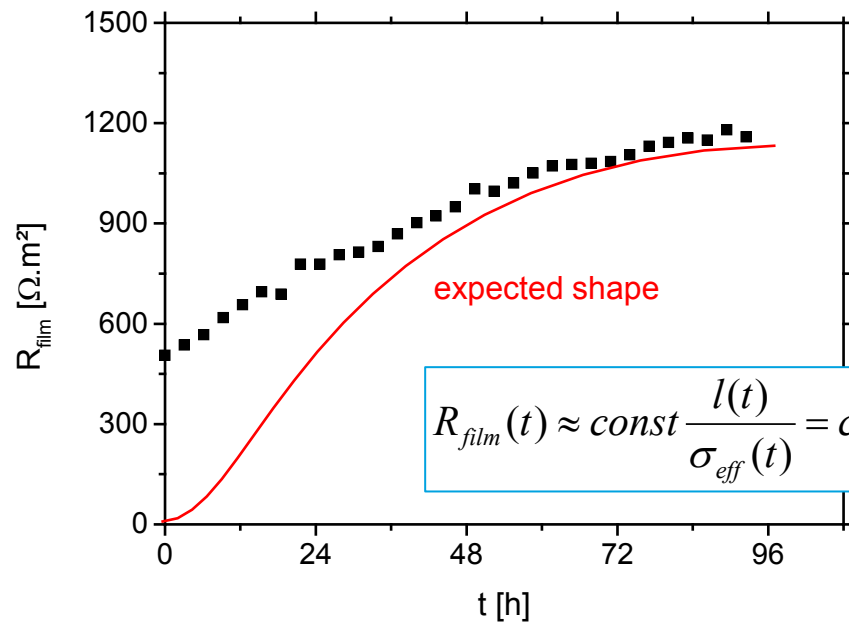
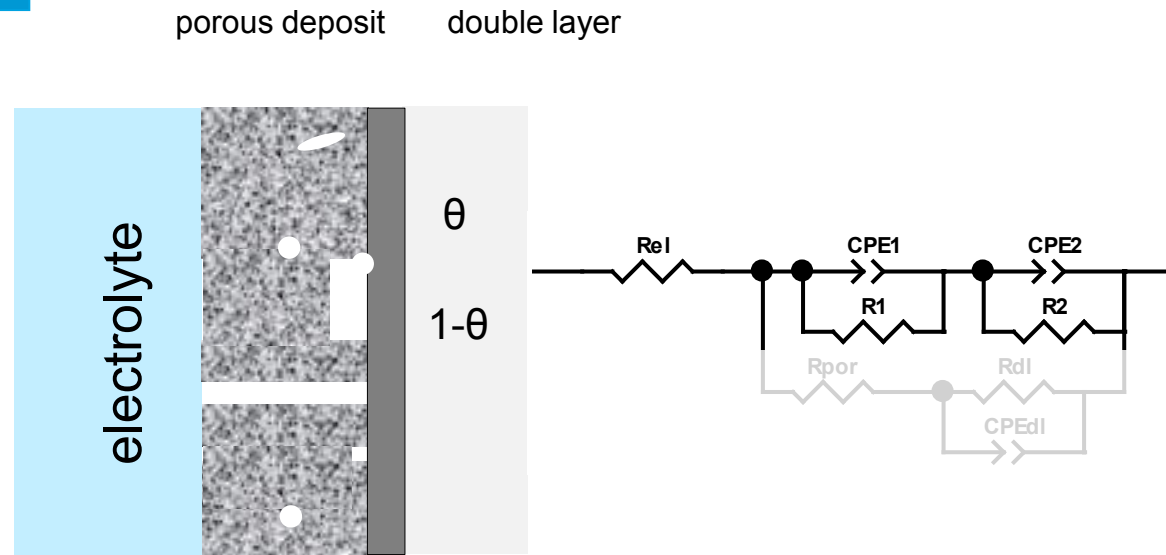
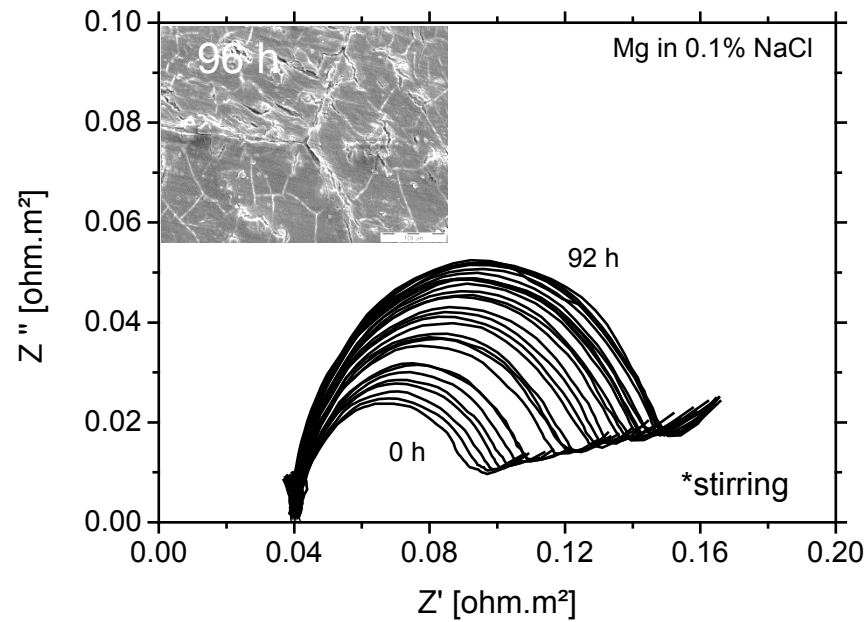
anodic dissolution

deposit growth

Assumptions and limitations

- Al is non-corroding (anodic branch is neglected)
- dilute solution theory is applicable
- precipitates do not dissolve
- hydroxide formation occurs at the interface
- limited number of chemical specimens and reaction products
- non-technical alloys
- without localised effects (pitting / Cl⁻)
-

Results – checking the model



$$R_{film}(t) \approx const \frac{l(t)}{\sigma_{eff}(t)} = const \frac{l(t)}{\sigma \theta(t) s^n \epsilon^2}$$

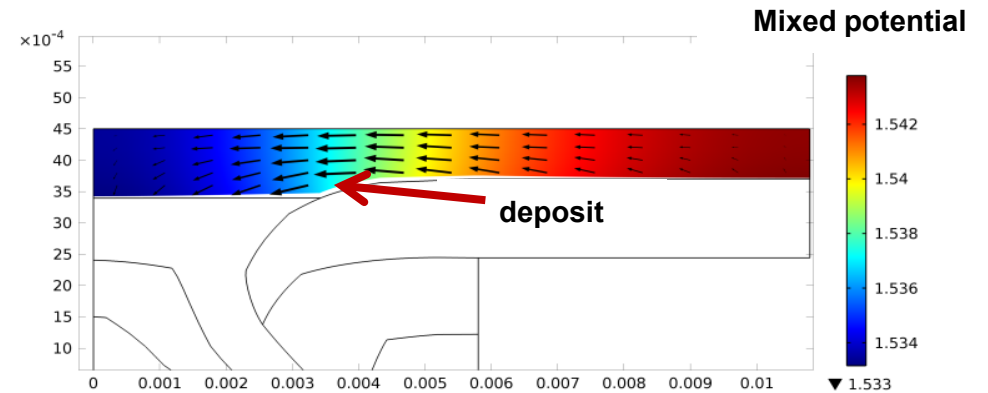
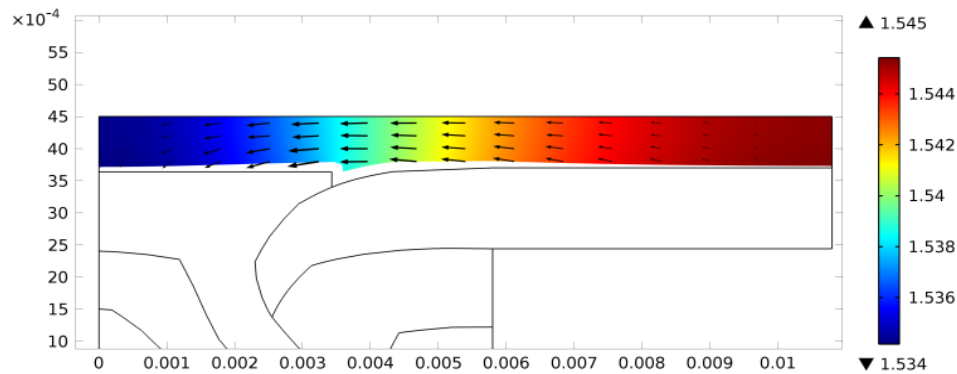


→ $\theta > 0$ at $t=0$ (native layer)

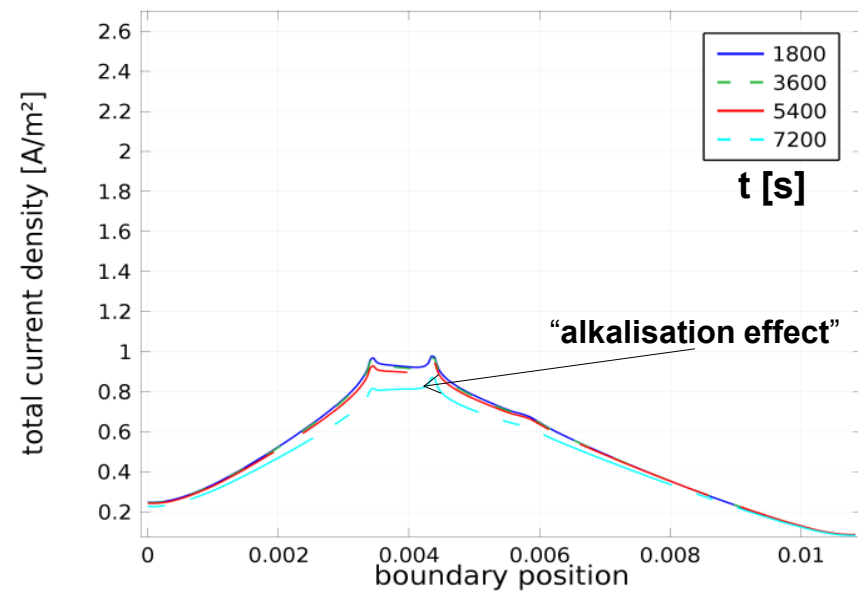
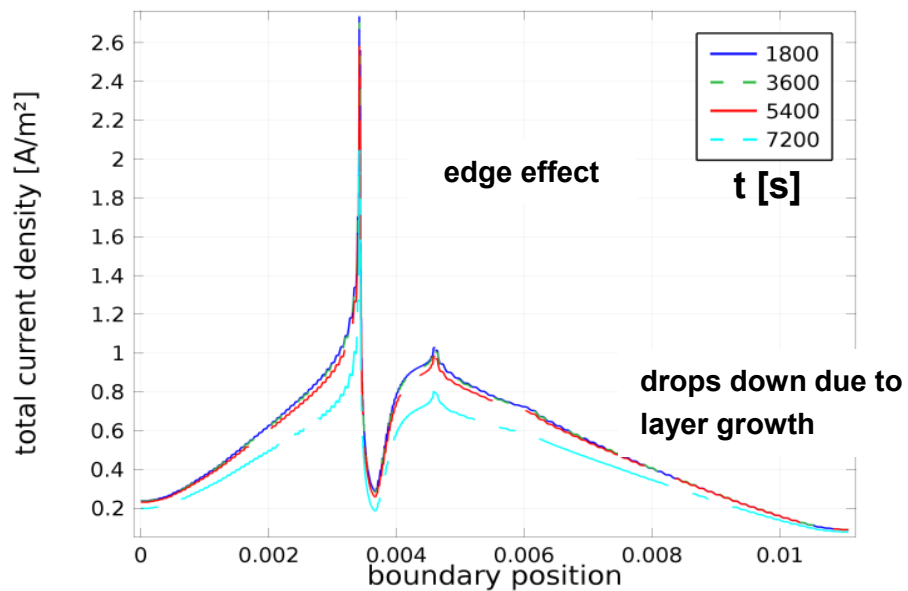
Results – Geometry aspects

first results without reducing flux:

e.g. different head shape:

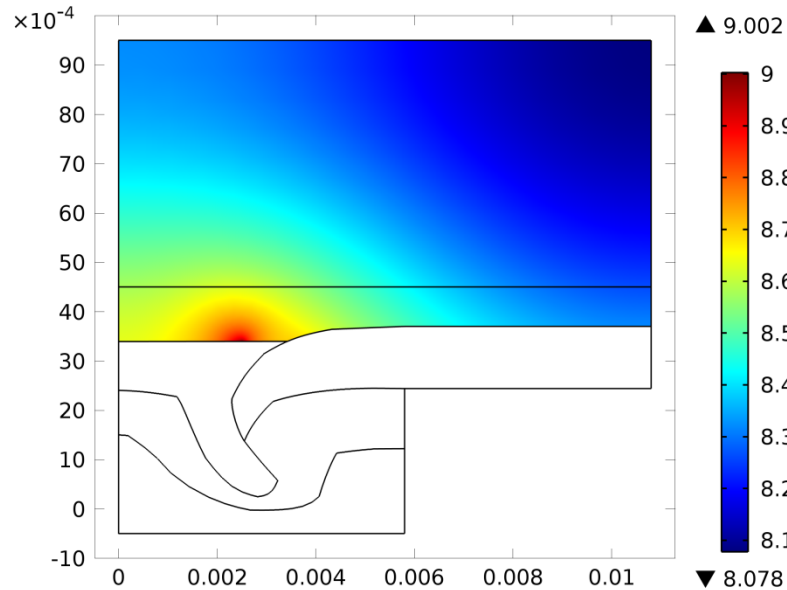


minimizing the corrosion current density:



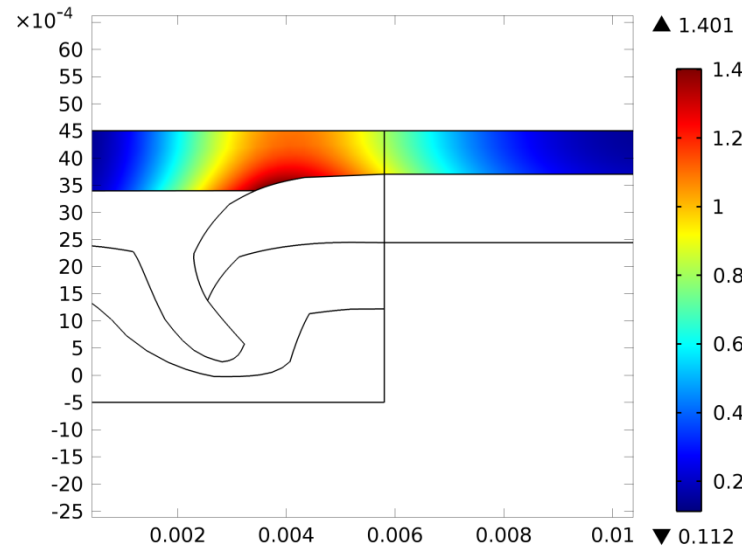
Results – Possible studies

pH - development



accelerating pre-developments and designing the layout

ion concentrations ($c_{\text{Mg}^{2+}}$ [mol/m³])



- Aspects of galvanic corrosion can be predicted
- Environmental exposure modelling still needs to be setup
- Surface treatments and coatings have to be tackled separately

Alloys...

Need of further extensions

- addition of further chemical specimens
- improved layer model including the MgO aspects
- predicting localised corrosion issues
- correlation to functionality (e.g. strength, stiffness)
- Al activity has to be taken into account especially at high pH values (>12 hydroxide species)
-

Results and issues of the model study

beside the previous explained aspects by Song et.al:

- sharp edges and gradients should be avoided due to local “critical” increases in the current density arising in discontinues anodic “dissolution” currents
- the relative position of the cathode should be “below” the anode to force precipitation of chemical products → decrease in the cathodic current
- $\theta=1$ for a non-porous structure would stop corrosion → **the engineer should try to find an alloy system achieving $(1 - \theta + \theta\varepsilon) \rightarrow 0$**

Modelling issues:

- physical and chemical correct time depended boundary conditions
- capacitive double layer, layer growth is still to strong, convective effects
- pH and conductivity variations / migration
- re - dissolution effects

Summary

- Simulations can **assist** the design regarding corrosion protection
- Chose of the model depends on requirements (careful)
- Simplified parameter studies are possible and can save experimental effort
- Many process parameters still have to be implemented
- The whole simulation based design approach requires interdisciplinary working and should be tackled in modules

 **there is still much to do**

Thank you