

Heat and Mass Transfer Modelling during Freezing of Foodstuffs

O. Rouaud¹, Q. T. Pham²

¹LUNAM Université, ONIRIS, CNRS, GEPEA, UMR 6144, Nantes, France,
²University of New South Wales, Sydney, Australia

Comsol Conference
October 10-12, Milan, Italy

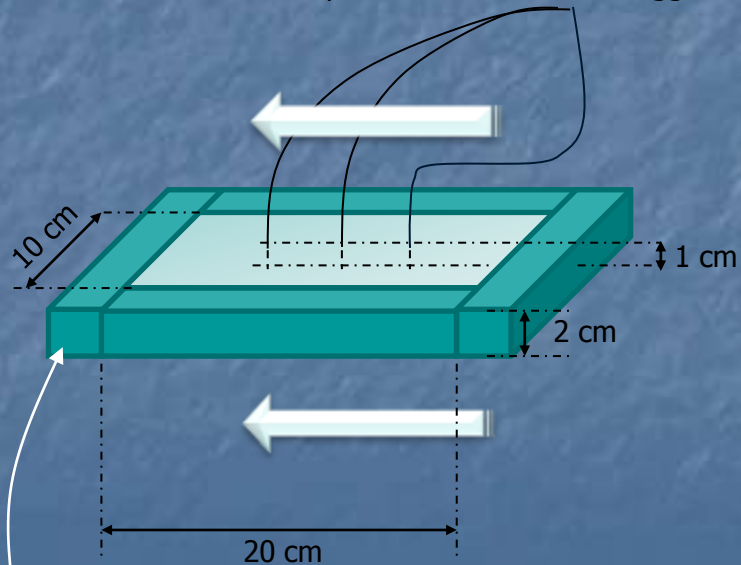
- To develop a mathematical model dedicated to the determination of freezing rate and weight loss during the freezing of food (*in very cold environment*).
- 2 freezing conditions studied:
 - Cryogenic device with Nitrogen gas at -80°C
 - Classical process with cold air at -30°C
- Comparisons with experimental data (cryogenic freezing)
- Focus on the influences of the external temperature and on the heat transfer coefficient

Experiments

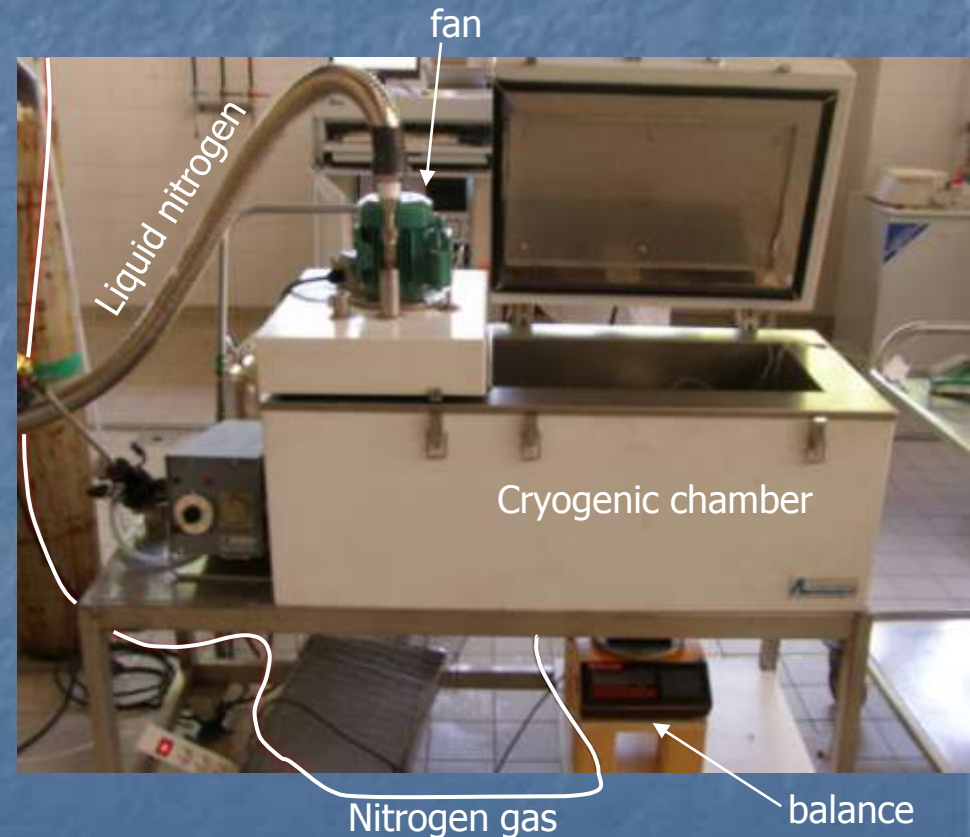
- Freezing of flat plate in an air-blast freezer
- Freezing of plate in a cryogenic chamber (-80°C)

Flat plate of methylcellulose gel with 3 thermocouples inside:

thermocouples connected to data logger



Polystyren foam

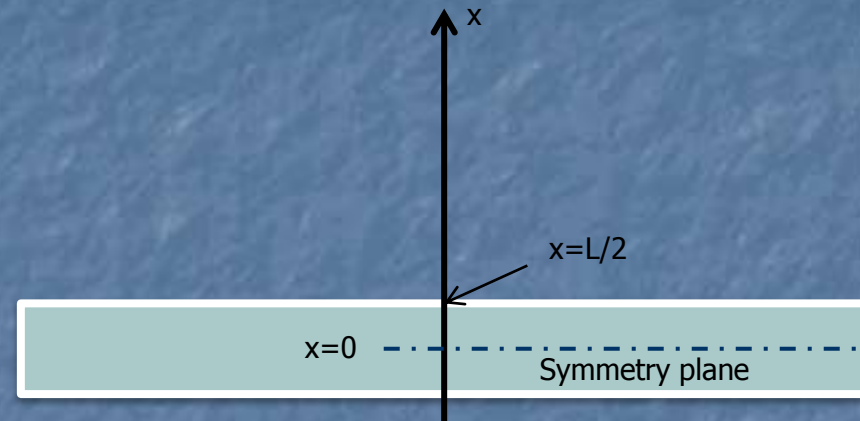


Experimental set-up

➤ 1D Heat Transfer

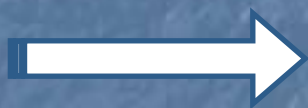
$$1) \quad \rho_{s,app} C_{p,app} \frac{\partial T}{\partial t} = \nabla \cdot (k_{eff} \nabla T)$$

$$2) \quad C_{p,app} = C_s + X_l C_l + X_{ice} C_{ice} - H_{li} \frac{\partial X_{ice}}{\partial T}$$



➤ 1D Mass Transfer

$$3) \quad \rho_{s,app} \frac{\partial X}{\partial t} = \nabla \cdot (\rho_{s,app} D_{eff} \nabla X_l) \quad \text{with} \quad X_l = X - X_{ice} \quad \text{and} \quad X_{ice} = (X - X_b) f(T)$$



$$\rho_{s,app} \frac{\partial X}{\partial t} = \nabla \cdot \left(\rho_{s,app} D_{eff} \left[(1 - f(T)) \nabla X + (X_b - X) \frac{df}{dT} \nabla T \right] \right)$$

➤ Function that takes into account the ice formation:

$$f(T) = 1 - \left(\frac{T_f - 273.15}{T - 273.15} \right) \left(\frac{T - T_{ff}}{T_f - T_{ff}} \right) \quad \text{if } T_{ff} \leq T \leq T_f ; \quad 0 \text{ if } T > T_f ; \quad 1 \text{ if } T < T_{ff}$$

➤ Boundary conditions:

- Evaporation (and sublimation) at the surface of food ($x=L/2$)
- 1 plane of symmetry ($x=0$)

$$\left(-k_{\text{eff}} \nabla T\right) = 0 \quad \text{at } x = 0$$

$$\left(-k_{\text{eff}} \nabla T\right) = h(T - T_{\text{amb}}) + F_w (H_{\text{vl}} + f_{\text{ice}} H_{\text{li}}) \quad \text{at } x = L / 2$$

$$\left(\rho_{s,\text{app}} D_{\text{eff}} \nabla X\right) = 0 \quad \text{at } x = 0$$

$$\left(\rho_{s,\text{app}} D_{\text{eff}} \nabla X\right) = -h_m \left(P_{\text{sat}} a_w - P_{\text{sat_amb}} RH\right) \quad \text{at } x = L / 2$$

➤ Initial and external conditions:

- Initial temperature and water content homogeneous inside the food
- External temperature (T_{amb}) and heat transfer coefficient (h) constant

- Implementation in Comsol 4.2
- Comsol interface: PDE interface chosen for the mass transfer

$$X \equiv u$$

$$f(T) \equiv \text{ice3} \equiv \text{ice}(T)$$

$$D_{\text{eff}} \equiv D_w$$

$$\rho_{s,\text{app}} \equiv \rho_{\text{MS}}$$

- ice(T) defined as analytic function in Model/Definitions
- Derivative of f(T) computed by Comsol:

$$\frac{df}{dT} \equiv d(\text{ice3}, T)$$

Equation

Show equation assuming:

Study 1, Time Dependent

$$e_a \frac{\partial^2 u}{\partial t^2} + d_a \frac{\partial u}{\partial t} + \nabla \cdot (-c \nabla u - \alpha u + \gamma) + \beta \cdot \nabla u + a u = f$$

$$\nabla = \left[\frac{\partial}{\partial x} \right]$$

Diffusion Coefficient

c kg/(m·s)

Absorption Coefficient

Source Term

Mass Coefficient

Damping or Mass Coefficient

d_a kg/m³

Conservative Flux Convection Coefficient

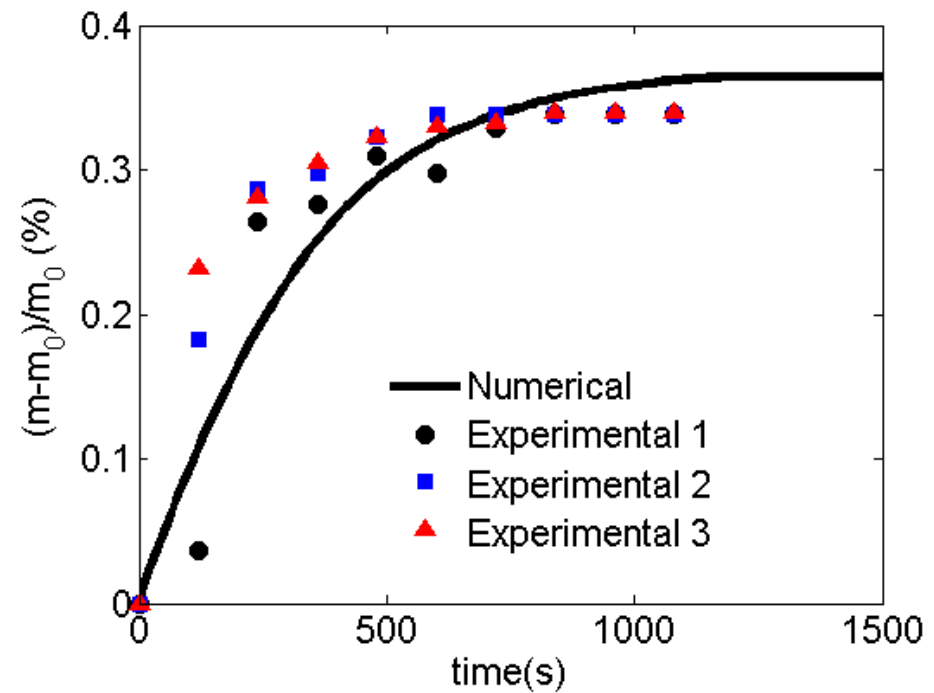
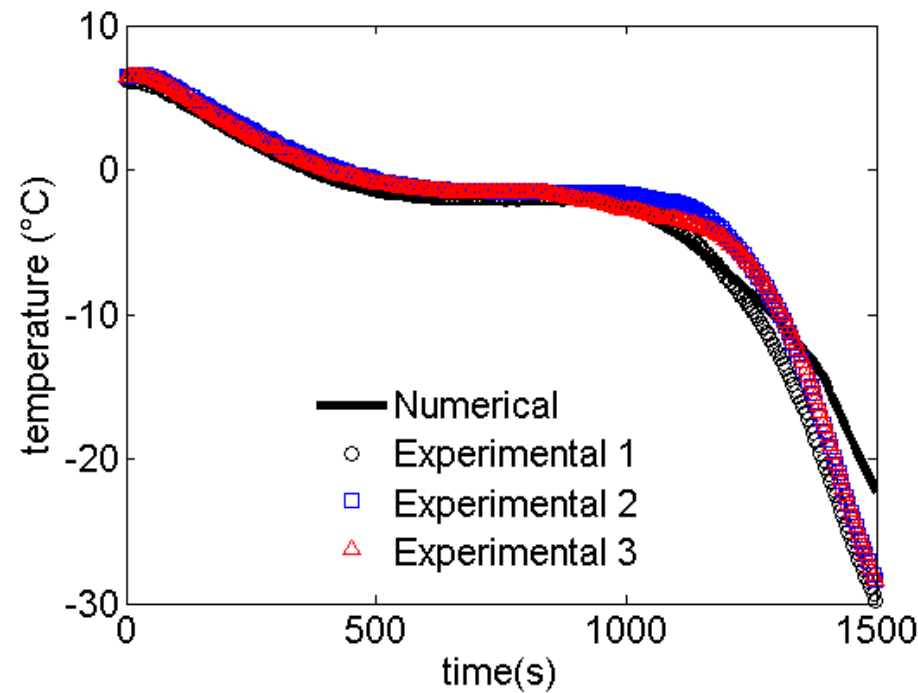
α kg/(m²·s)

Convection Coefficient

Conservative Flux Source

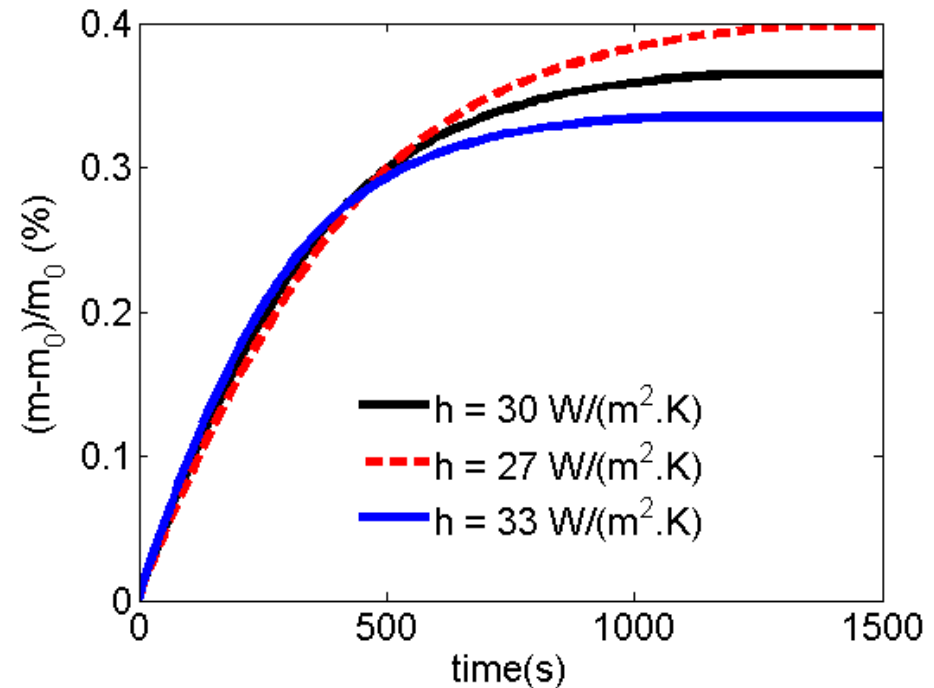
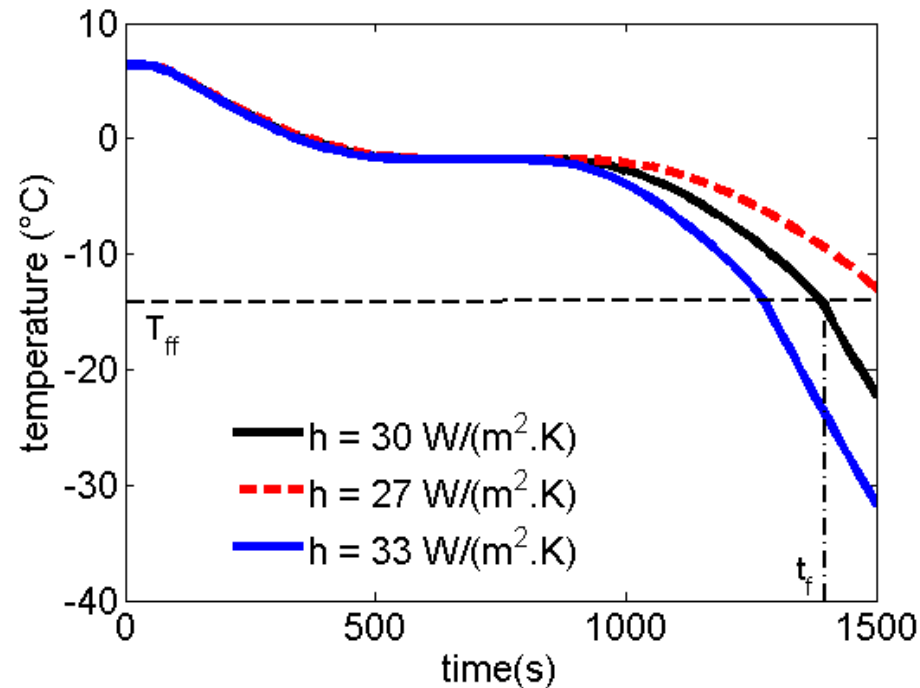
γ kg/(m²·s)

- Comparison between numerical and experimental results in the cryogenic system ($T_{amb} = -80^{\circ}\text{C}$, $h = 30 \text{ W}\cdot\text{m}^{-2}\cdot\text{K}^{-1}$)



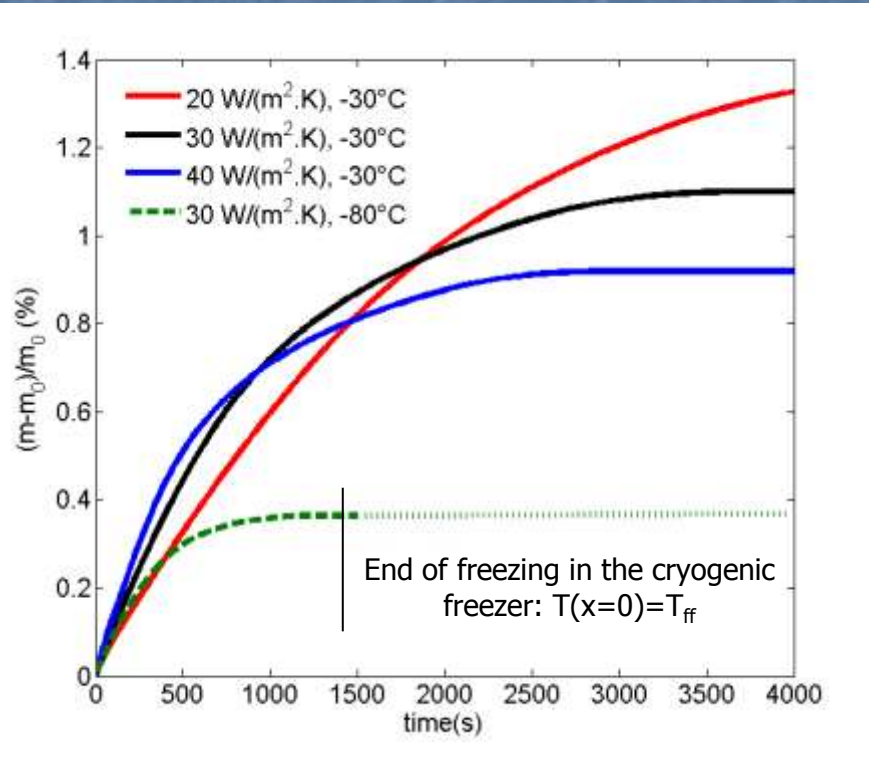
- Temperature well predicted despite freezing time slightly underestimated
- Good agreement between simulated and experimental weight loss

➤ Influence of the heat transfer coefficient



- Increasing h by 10% decreases the effective freezing time t_f by 9% (t_f : from T_i to T_{ff})
- Increasing h by 10% decreases the mass loss by 8%.

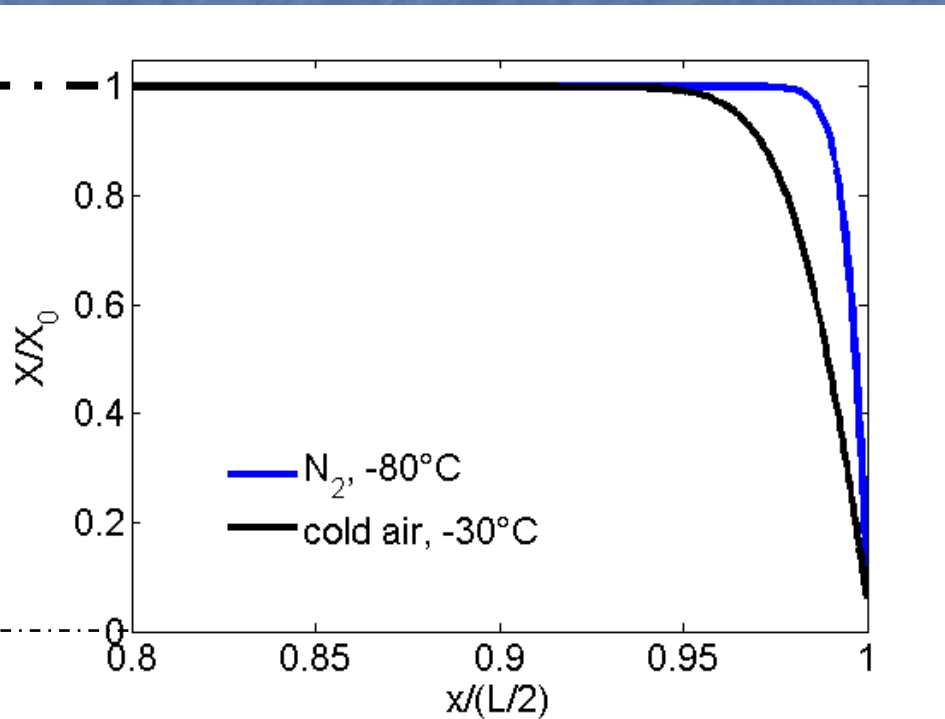
➤ Cryogenic freezing vs air-blast freezing



- Effective freezing time in cold air is 3 times higher than in the cryogenic freezer for the same h (4000 s vs 1400 s)
- Air-blast freezing: the weight loss is higher at the beginning (chilling) if h is higher
- The total weight loss at the end of freezing is less for high heat transfer coefficient because T_f is reached sooner

- The weight loss is reduced in cryogenic freezer due to the very low temperature (less than 0.4% vs 1.1% for air-blast freezing)

- Strong water content gradient at the surface:
 - Finer grid essential close to the surface ($\delta x \approx 1.e-5$ m)



- Phase change characterized by a sharp peak ($C_{p,app}(T)$):
 - Using the time dependent solver with free time steps limited to 1s to ensure the recognition of the phase change.
- Problems with discontinuities at $T = T_{ff}$ due to the function $f(T)$
- Experiments: strong influence of experimental conditions (h , central temperature...)

Conclusion

- Development of a mathematical model to predict the freezing time and the weight loss of food during freezing
- Model developed for non-porous food, well suited for freezing in very low ambient temperatures (high heat and mass transfer):
 - Agreement between experimental and numerical results
- Using very cold environment reduces the freezing time and the weight loss
- High degree of dehydration at the beginning (chilling) – sublimation negligible
- Perspectives:
 - Model will be developed for porous food
 - The function $f(T)$ has to be improved



Thank you for your attention

